

# Thermodynamic approach to evaluating complexants for environmental performance assessment and decontamination

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# Objectives

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Discuss methodology to:

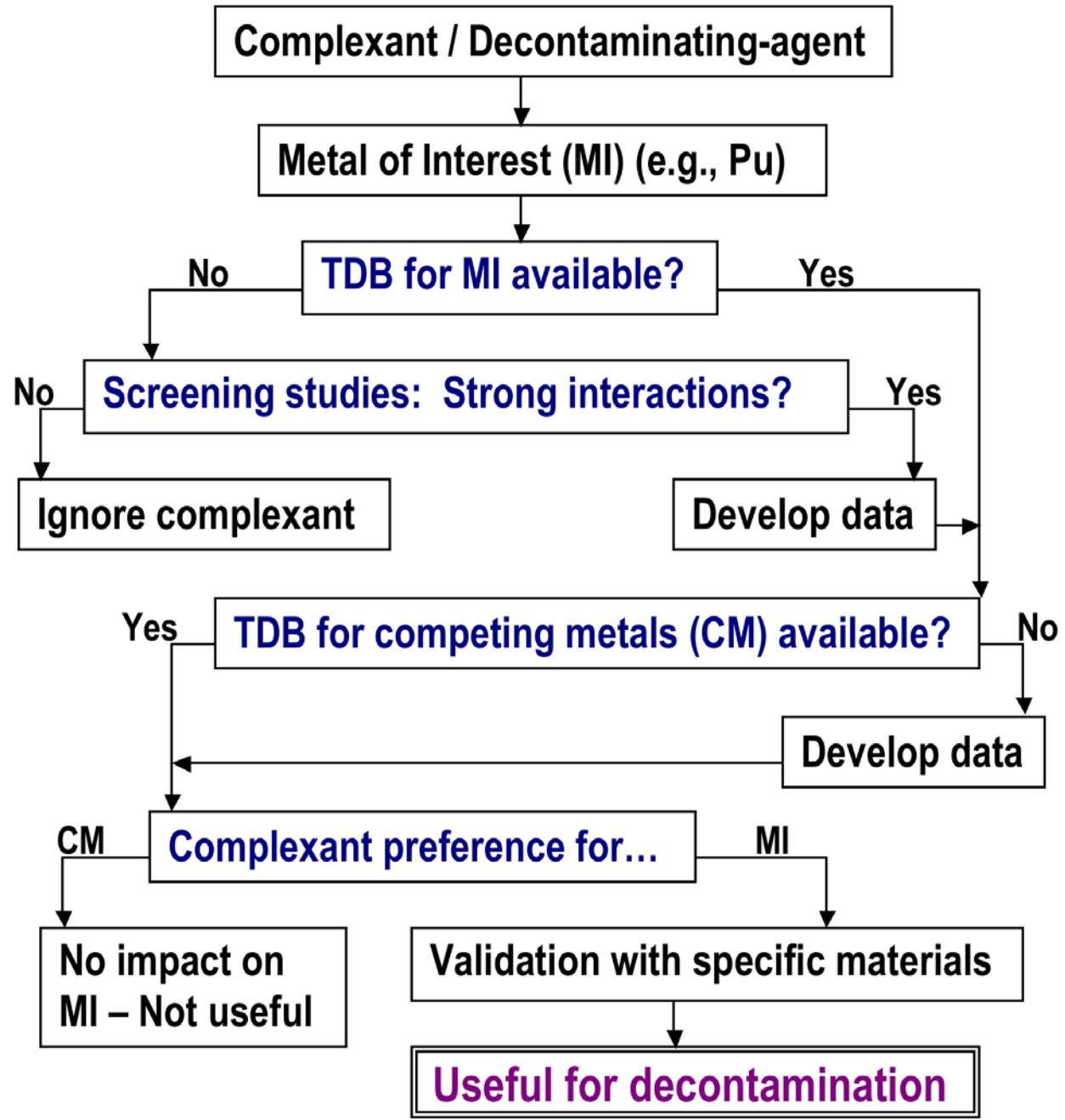
- Evaluate different complexants for their usefulness in decontamination
- Determine the influence of a given complexant on solubilization

# Discussion Format

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- General approach
- Using EDTA as an example discuss:
  - EDTA data needs for simple systems (e.g., Pu(IV), Fe(III), Ca)
  - Data validation in complex systems
  - Application of data to decontamination and PA
- Using ISA as an example discuss:
  - ISA data needs for simple systems (e.g., Th, Fe(III), Np(IV), Ca)
  - Application of data to decontamination and PA
- Brief summary

## Fundamental approach for selecting decontaminating agents



# Important aspects of general approach

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- Develop thermodynamic data in simple systems consistent with all of the available reliable data
- Validate data in complex systems (e.g., brines, in the presence of MI and CM)
- Evaluate whether a given ligand will increase solubility or be useful for decontamination, which will depend on relative:
  - Values of complexation constants
  - Metal ion activities

# Example: Pu(IV)-EDTA

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Using fundamental data determine whether EDTA can:

- Make Pu(IV) mobile in geologic environments
- Be used for Pu(IV) decontamination activities

# Factors governing EDTA-mediated Pu mobility or decontaminating ability

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- Oxidation state of Pu
- pH
- EDTA concentration in solution, which depends on
  - Total amount disposed or used
  - Microbial degradation
  - Adsorption
- Competing metal ions (e.g.,  $\text{Ca}^{2+}$ ,  $\text{Fe}^{3+}$ ,  $\text{Al}^{3+}$ ,  $\text{Mg}^{2+}$ )
  - Complexation constants
  - Activities of bare ions

# Thermodynamic data for EDTA complexes

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Prior to our study [Rai et al. 2008], reliable data were not available for:

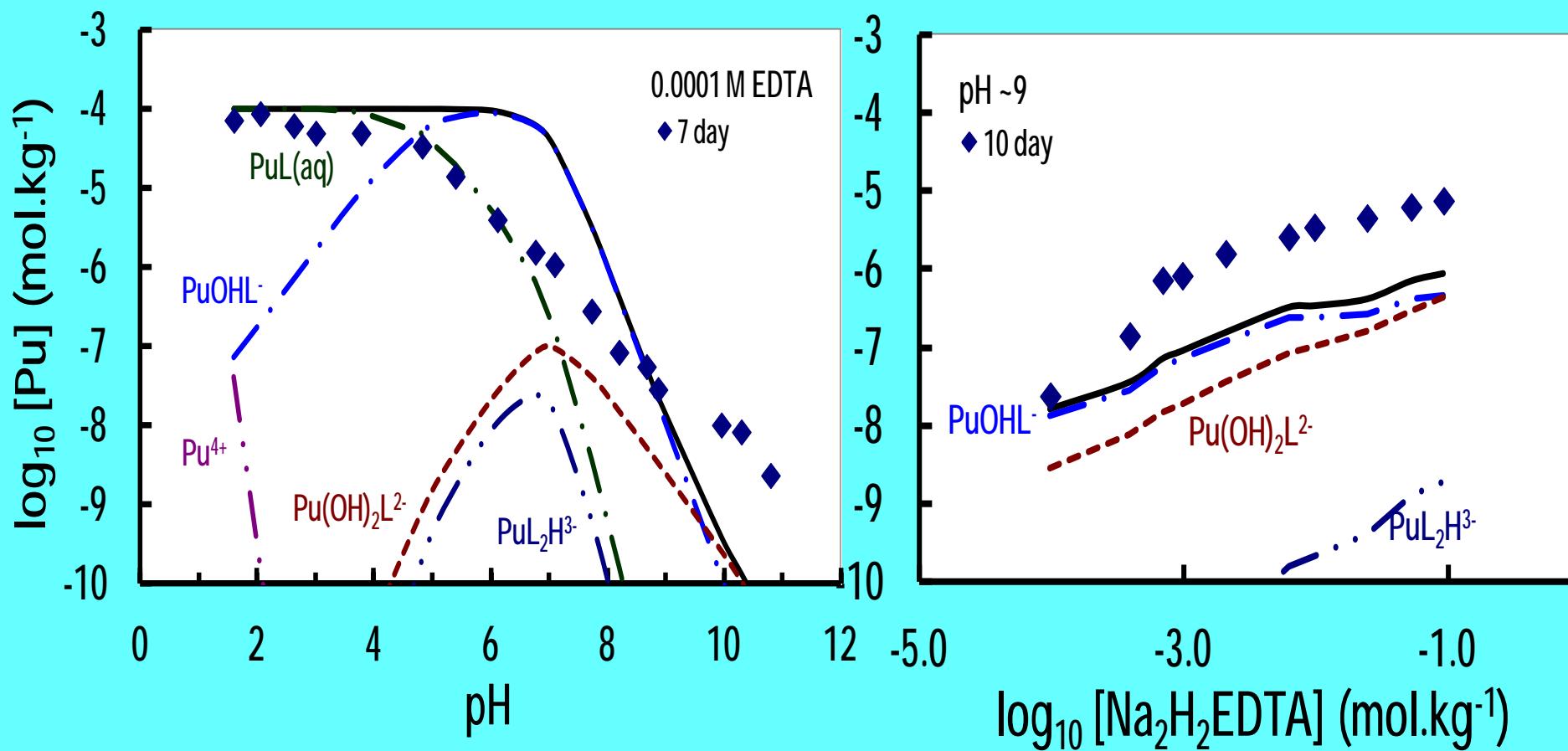
□ Pu(IV)-EDTA

- Large number of species proposed [ $\text{Pu(OH)EDTA}^-$ ,  $\text{Pu(OH)}_2\text{EDTA}^{2-}$ ,  $\text{Pu(OH)}_3\text{EDTA}^{3-}$ ,  $\text{PuEDTA(aq)}$ ,  $\text{PuHEDTA}^+$ ,  $\text{Pu(EDTA)}_2^{4-}$ ,  $\text{PuH(EDTA)}_2^{3-}$ ,  $\text{PuH}_3(\text{EDTA})_2^-$ ]
- Poor quality data with large variability

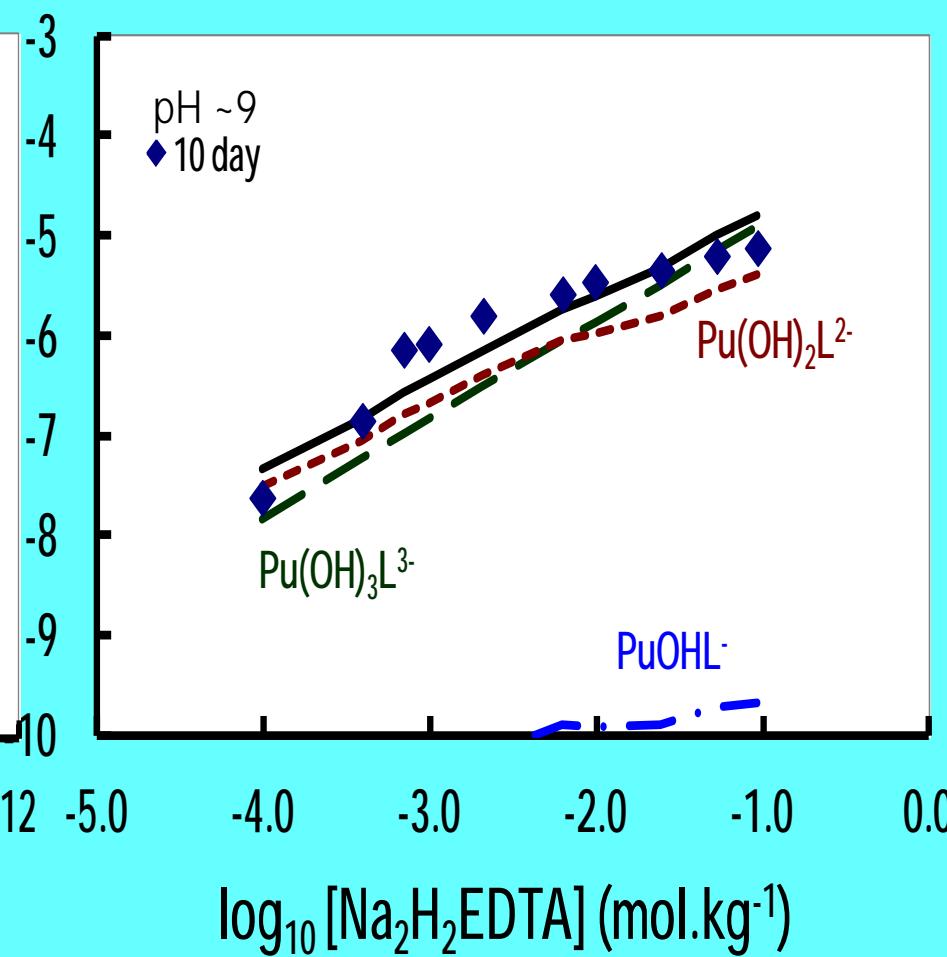
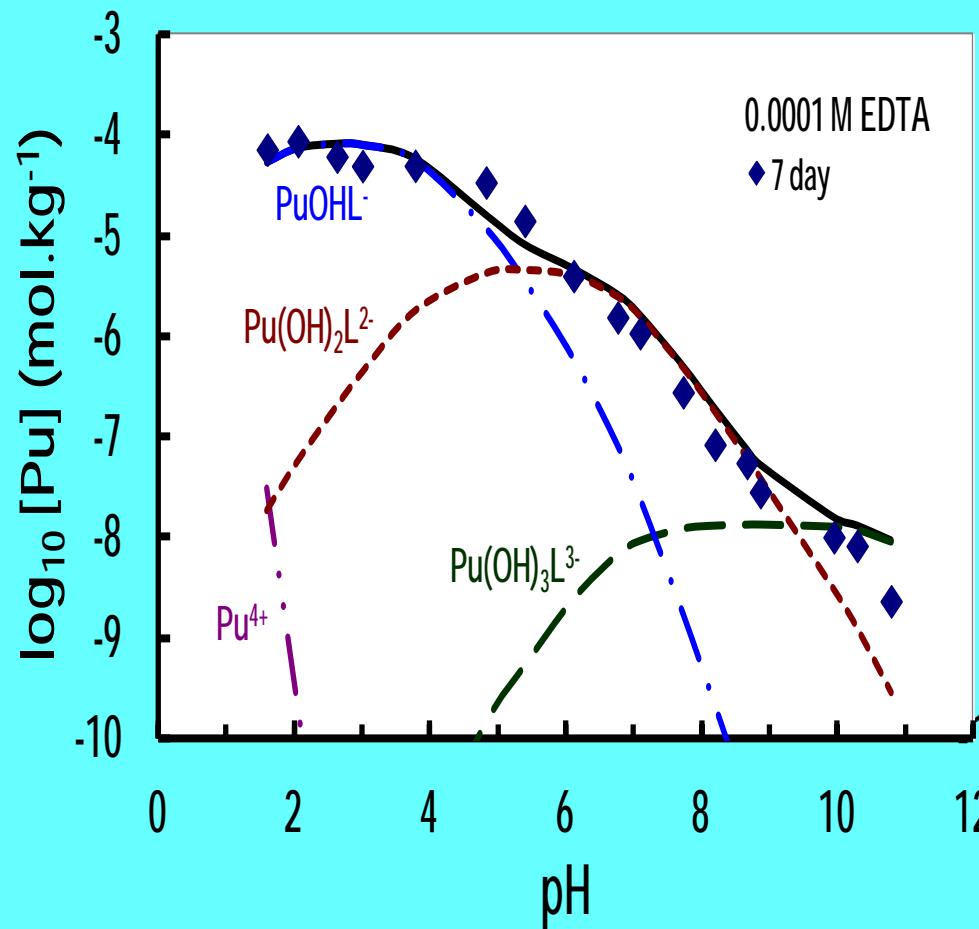
□ Fe(III)) with OH and EDTA

- Large number of hydroxide species proposed [ $\text{FeOH}^{2+}$ ,  $\text{Fe(OH)}_2^+$ ,  $\text{Fe(OH)}_4^-$ ,  $\text{Fe}_2(\text{OH})_2^{4+}$ ,  $\text{Fe}_3(\text{OH})_4^{5+}$ ]
- Large number of EDTA species proposed [ $\text{FeEDTA}^-$ ,  $\text{Fe(OH)EDTA}^{2-}$ ,  $\text{Fe}_2(\text{OH})_2(\text{EDTA})_2^{4-}$ ,  $\text{FeHEDTA(aq)}$ ]
- Poor quality data with large variability

# Comparison of experimental PuO<sub>2</sub>(am) solubility (Rai et al. 2001) to the literature model (Rai et al. 2008)



# Thermodynamic interpretations of $\text{PuO}_2(\text{am})$ solubility data (Rai et al. 2008)



# Important Pu(IV)-EDTA species

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Literature	Rai et al. 2008
Pu(OH)EDTA <sup>-</sup>	Pu(OH)EDTA <sup>-</sup>
Pu(OH) <sub>2</sub> EDTA <sup>2-</sup>	Pu(OH) <sub>2</sub> EDTA <sup>2-</sup>
Pu(OH) <sub>3</sub> EDTA <sup>3-</sup>	Pu(OH) <sub>3</sub> EDTA <sup>3-</sup>
PuEDTA(aq)	NR
PuHEDTA <sup>+</sup>	NR
Pu(EDTA) <sub>2</sub> <sup>4-</sup>	NR
PuH(EDTA) <sub>2</sub> <sup>3-</sup>	HR
PuH <sub>3</sub> (EDTA) <sub>2</sub> <sup>-</sup>	NR
NR = Not required	

# Thermodynamic data for EDTA complexes

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Prior to our study [Rai et al. 2008], reliable data were not available for:

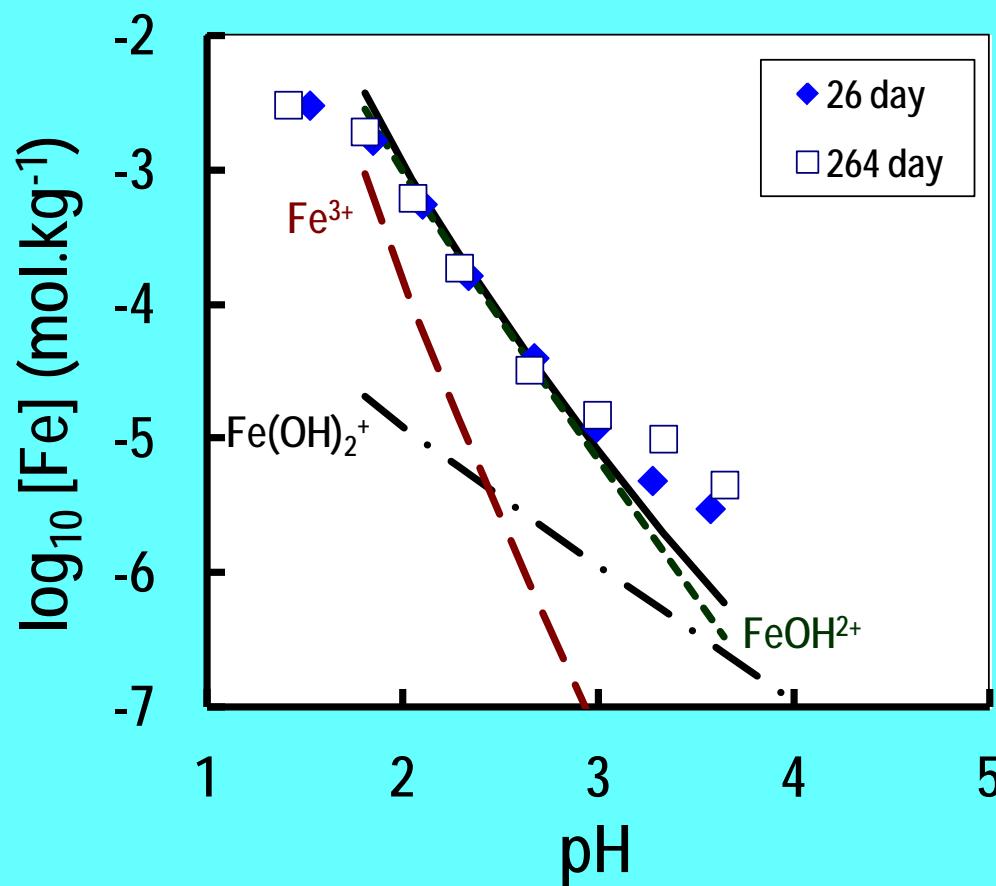
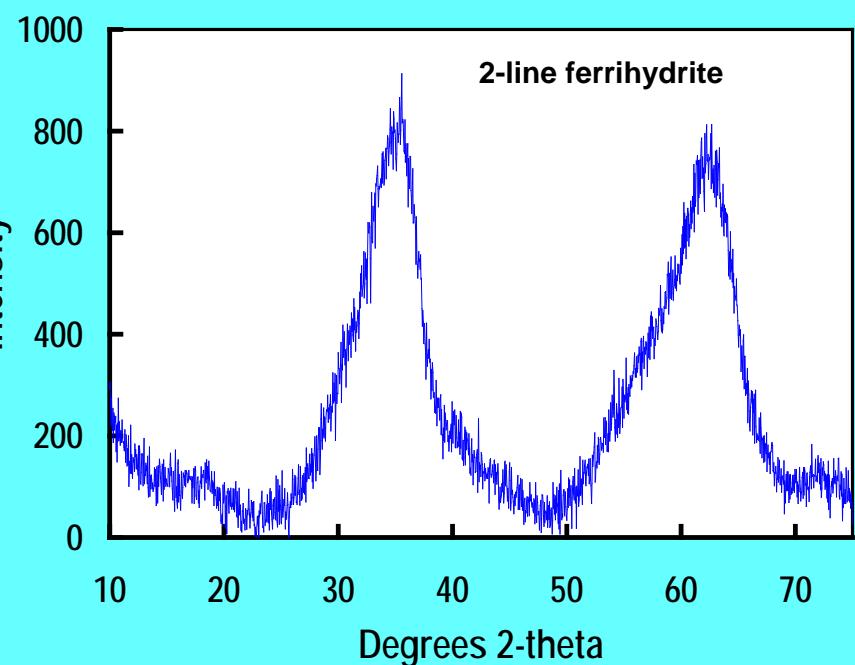
□ Pu(IV)-EDTA

- Large number of species proposed [ $\text{Pu}(\text{OH})\text{EDTA}^-$ ,  $\text{Pu}(\text{OH})_2\text{EDTA}^{2-}$ ,  $\text{Pu}(\text{OH})_3\text{EDTA}^{3-}$ ,  $\text{PuEDTA(aq)}$ ,  $\text{PuHEDTA}^+$ ,  $\text{Pu}(\text{EDTA})_2^{4-}$ ,  $\text{PuH}(\text{EDTA})_2^{3-}$ ,  $\text{PuH}_3(\text{EDTA})_2^-$ ]
- Poor quality data with large variability

□ Fe(III)) with OH and EDTA

- Large number of hydroxide species proposed [ $\text{FeOH}^{2+}$ ,  $\text{Fe}(\text{OH})_2^+$ ,  $\text{Fe}(\text{OH})_4^-$ ,  $\text{Fe}_2(\text{OH})_2^{4+}$ ,  $\text{Fe}_3(\text{OH})_4^{5+}$ ]
- Large number of EDTA species proposed [ $\text{FeEDTA}^-$ ,  $\text{Fe}(\text{OH})\text{EDTA}^{2-}$ ,  $\text{Fe}_2(\text{OH})_2(\text{EDTA})_2^{4-}$ ,  $\text{FeHEDTA(aq)}$ ]
- Poor quality data with large variability

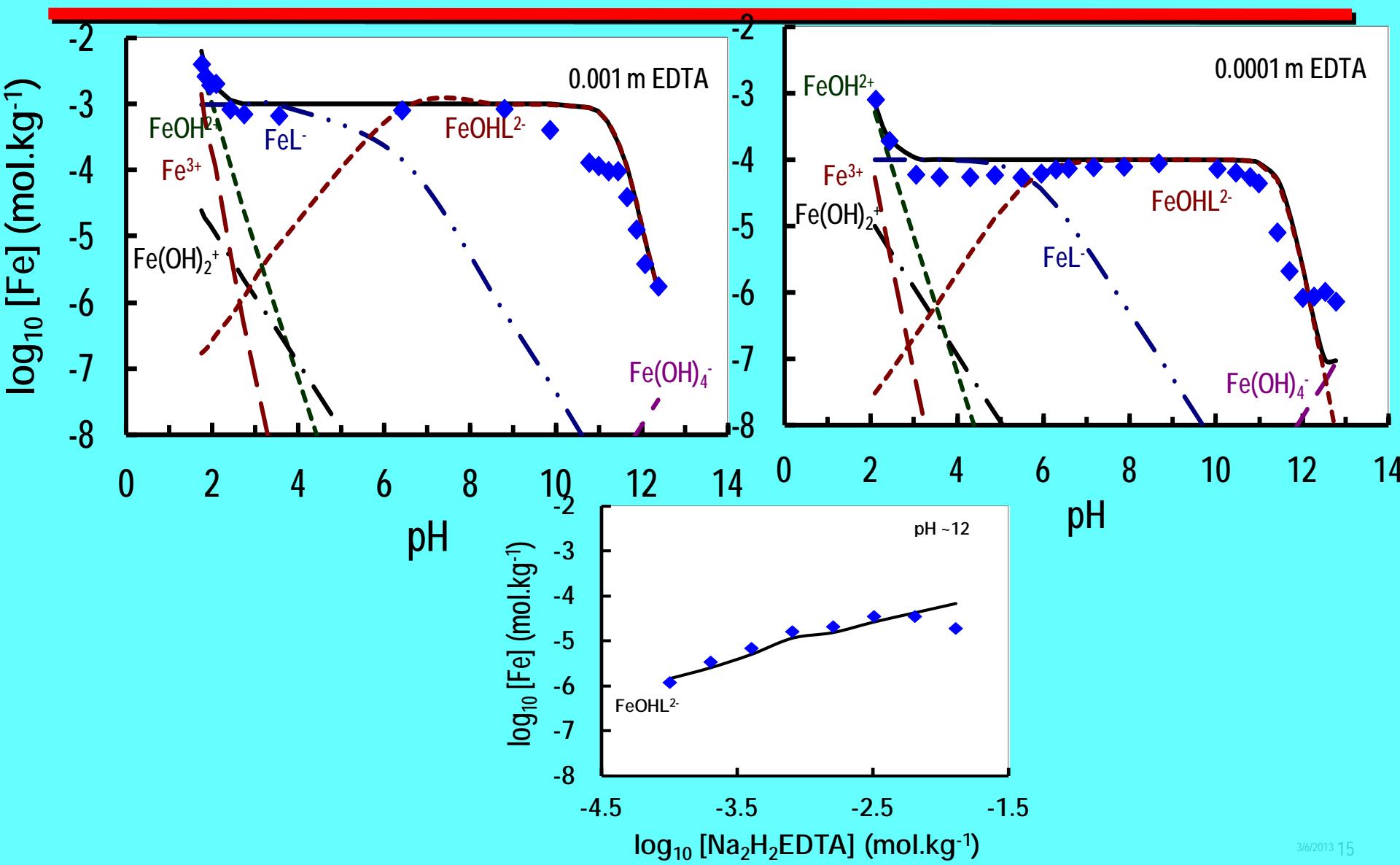
# $\text{Fe(OH)}_3(\text{s})$ solubility as a function of pH (Rai et al. 2008)



# Important Fe-EDTA species

Literature	Rai et al. 2008
$\text{Fe(OH)}^{2+}$	$\text{Fe(OH)}^{2+}$
$\text{Fe(OH)}_2^{2+}$	$\text{Fe(OH)}_2^{2+}$
$\text{Fe(OH)}_4^-$	$\text{Fe(OH)}_4^-$
$\text{Fe}_2(\text{OH})_2^{4+}$	NR
$\text{Fe}_3(\text{OH})_4^{5+}$	NR
NR = Not required	

# $\text{Fe(OH)}_3(\text{am})$ solubility as a function of pH and EDTA (Rai et al. 2008)



# Important Fe-EDTA species

Literature	Rai et al. 2008
$\text{Fe(EDTA)}^-$	$\text{Fe(EDTA)}^-$
$\text{FeOH(EDTA)}^{2-}$	$\text{FeOH(EDTA)}^{2-}$
$\text{Fe}_2(\text{OH})_2(\text{EDTA})_2^{4-}$	NR
$\text{FeH(EDTA)(aq)}$	NR
NR = Not required	

# Recommended values for EDTA complexes (Rai et al. 2008)

Reaction	$\log_{10} K^o$
$\text{Fe(OH)}_3(\text{s}) = \text{Fe}^{3+} + 3\text{OH}^-$	$-40.35 \pm 0.5$
$\text{Fe}^{3+} + \text{OH}^- = \text{FeOH}^{2+}$	$11.81 \pm 0.5$
$\text{Fe}^{3+} + \text{EDTA}^{4-} = \text{Fe(EDTA)}^-$	$27.66 \pm 0.209$
$\text{Fe}^{3+} + \text{EDTA}^{4-} + \text{H}_2\text{O} = \text{FeOH(EDTA)}^{2-} + \text{H}^+$	$21.935 \pm 0.226$
$\text{Pu}^{4+} + \text{EDTA}^{4-} + \text{OH}^- = \text{Pu(OH)EDTA}$	$38.422 \pm 0.258$
$\text{Pu}^{4+} + \text{EDTA}^{4-} + 2\text{OH}^- = \text{Pu(OH)}_2\text{EDTA}^{2-}$	$47.093 \pm 0.258$
$\text{Pu}^{4+} + \text{EDTA}^{4-} + 3\text{OH}^- = \text{Pu(OH)}_3\text{EDTA}^{3-}$	$51.769 \pm 0.258$
$\text{Ca}^{2+} + \text{EDTA}^{4-} = \text{CaEDTA}^{2-}$	$12.36^a$

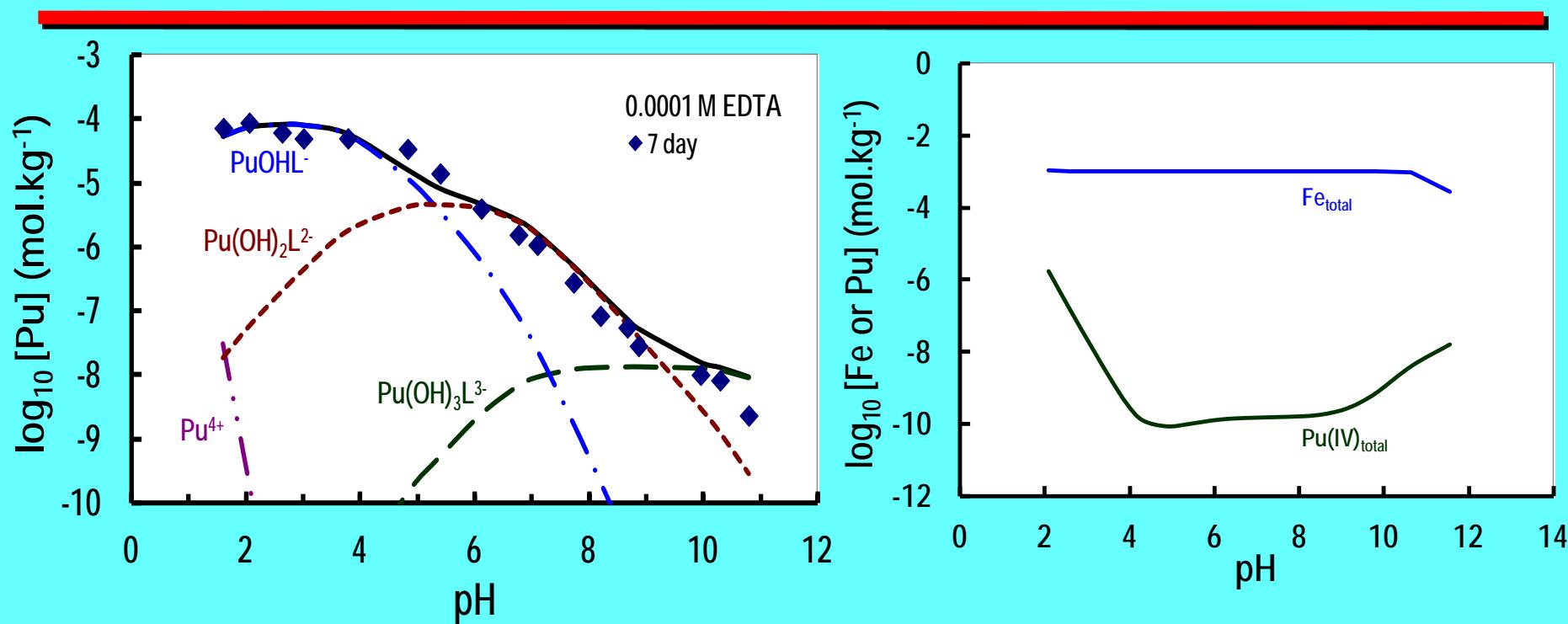
<sup>a</sup> Value from Felmy and Mason (2003)

# Impact of Fe(III) and Ca on Pu(IV) behavior in the presence of EDTA

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- Iron and Ca are very common in geologic environments
- Thermodynamic data for Pu(IV), Fe(III), and Ca are now available
- Use thermodynamic data to predict potential Pu(IV):
  - Mobility in the presence of EDTA and Fe(III) and Ca
  - Decontamination with EDTA in the presence of Fe(III) and Ca

# $\text{PuO}_2$ solubility in the presence of $\text{Fe(OH)}_3(\text{s})$ and 0.001 M EDTA (Rai et al. 2008)



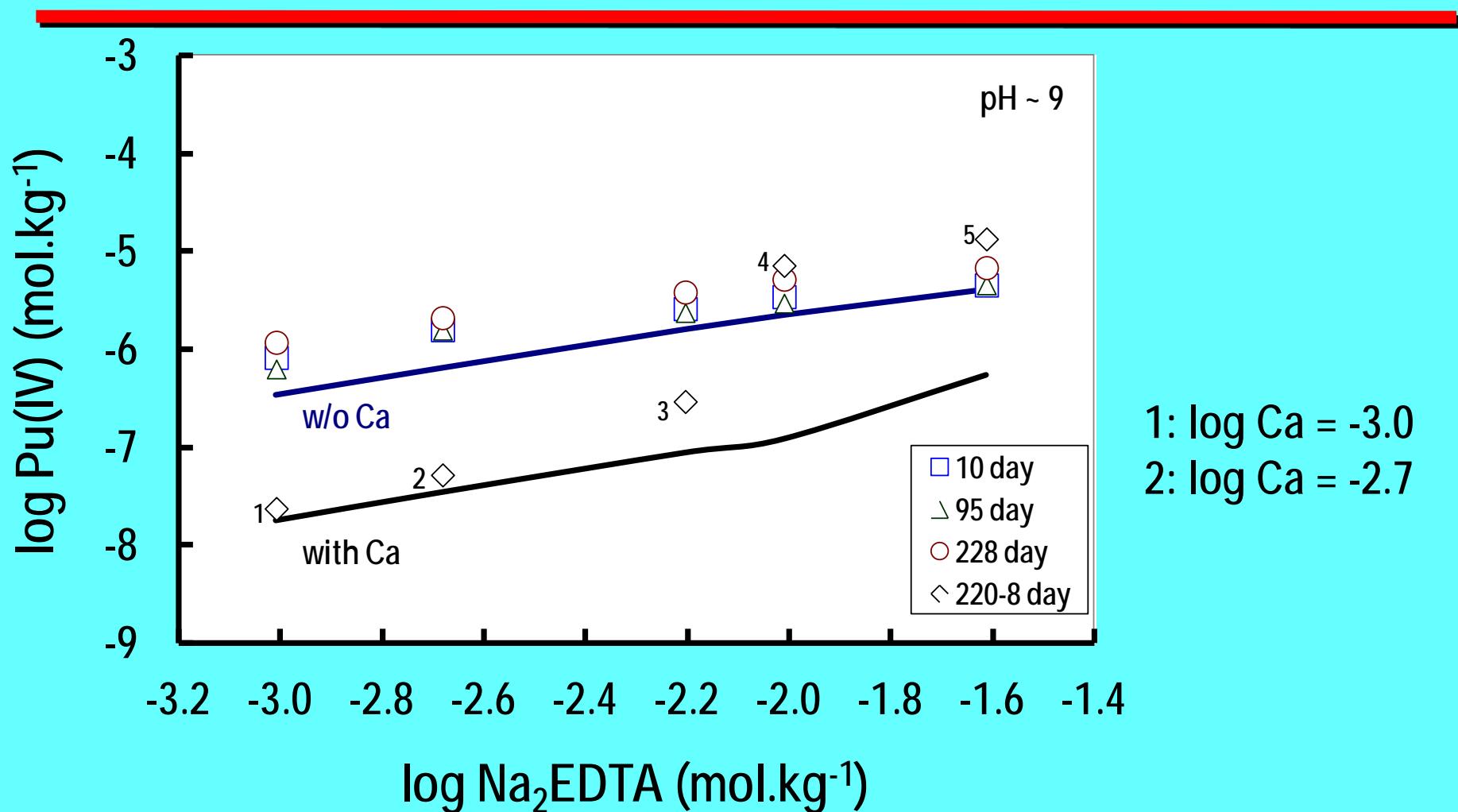
# Why does Fe(III) out competes Pu(IV) for EDTA binding?

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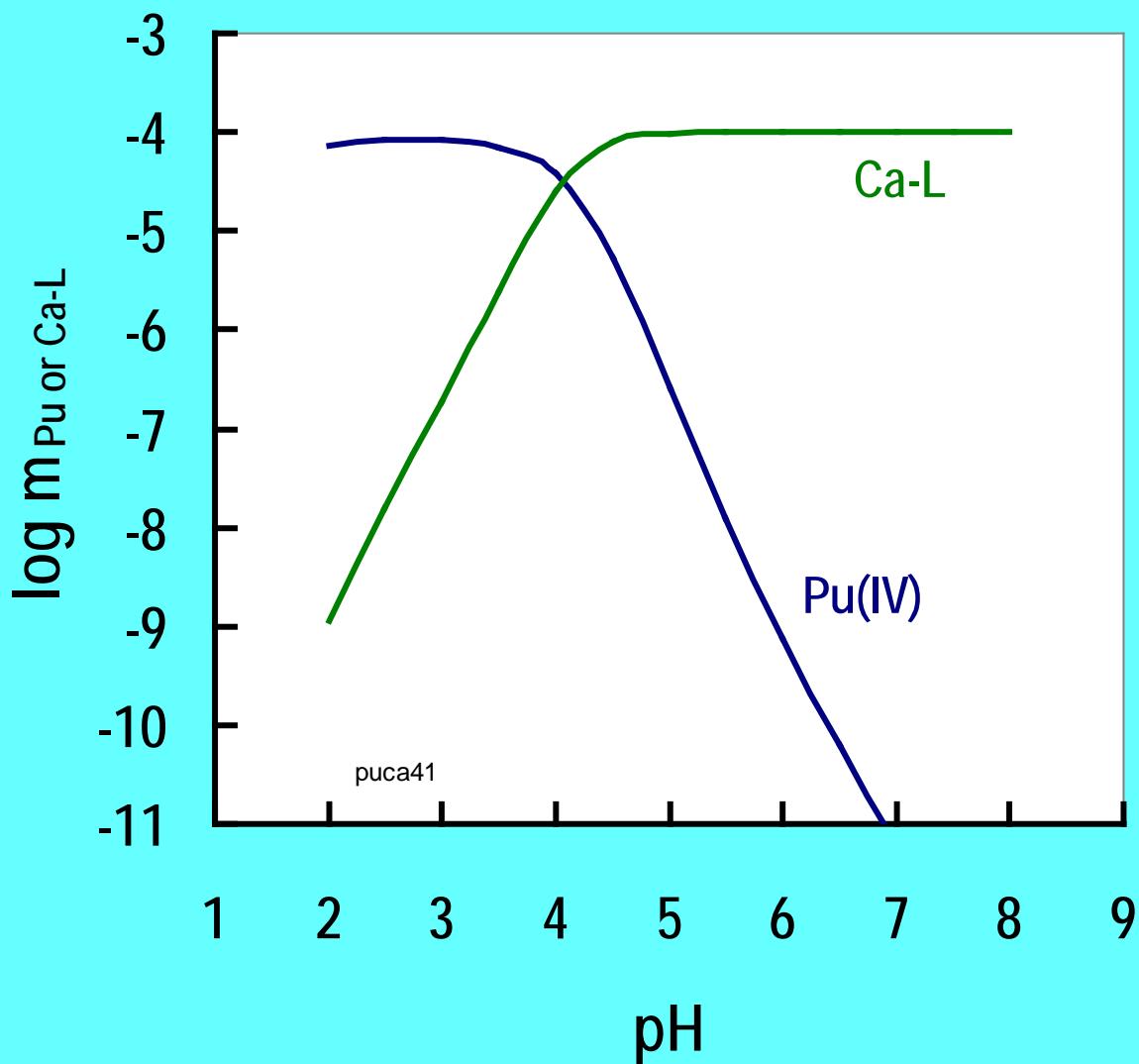
It is because of both

- Relativley stronger complexation constant
  - $\log K_{\text{FeEDTA}^-} = 27.66$
  - $\log K_{\text{PuEDTA}^0} \sim 26$
- Higher bare ion activity
  - $\log K_{\text{Fe}^{3+}} = 1.65 - 3\text{pH}$
  - $\log K_{\text{Pu}^{4+}} = -2.3 - 4\text{pH}$

# Experimental evaluation of the effect of Ca on PuO<sub>2</sub>(am) solubility as a function of EDTA



# $\text{PuO}_2(\text{am})$ solubility in the presence of 0.001 M Ca and 0.0001 M EDTA



# Why does Ca out competes Pu(IV) for EDTA binding?

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- It is due to higher bare ion activity

- $\log K_{\text{Ca}}^{2+} \approx -3$

- $\log K_{\text{Pu}}^{4+} = -2.3 - 4\text{pH}$

Because of relatively higher bare ion activity Ca out competes  $\text{Pu}^{4+}$  for binding with EDTA even though the complexation constant for  $\text{PuEDTA}^0$  is over 13 orders of magnitude stronger than the  $\text{CaEDTA}^{2-}$

# Conclusions for Pu(IV)-EDTA

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EDTA is not expected to make Pu(IV) mobile and it is not desirable decontaminating agent for Pu(IV) in complex geologic systems which is contrary to previously long-held opinions.

Past opinions based on:

- Pu(IV) co-disposed with EDTA
- Pu(IV)-EDTA complexes implicated for Pu mobility in field studies [81CLE/REE; 82REE/CLE]
- EDTA complexes of Pu(V, VI) convert to Pu(IV) [57FOR/SMI; 73Cau/Gui; 96ALM/ ;98 REE/WYG]
- Pu(III) spontaneously converts to Pu(IV) [94RUS/QUI]
- EDTA forms strong complexes with Pu(IV) [57FOR/SMI; 73Cau/Gui]

# Discussion Format

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- General approach
- Using EDTA as an example discuss:
  - EDTA TDB needs for simple systems (e.g., Pu(IV), Fe(III), Ca)
  - TDB validation in complex systems
  - Application of TDB to decontamination and PA
- Using ISA as an example discuss:
  - ISA TDB needs for simple systems (e.g., Th, Fe(III), Np(IV), Ca)
  - Application of TDB to decontamination and PA
- Brief summary

# Literature Th-ISA model [2006ALL/EKB ] based on solvent extraction data

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## Modeling species

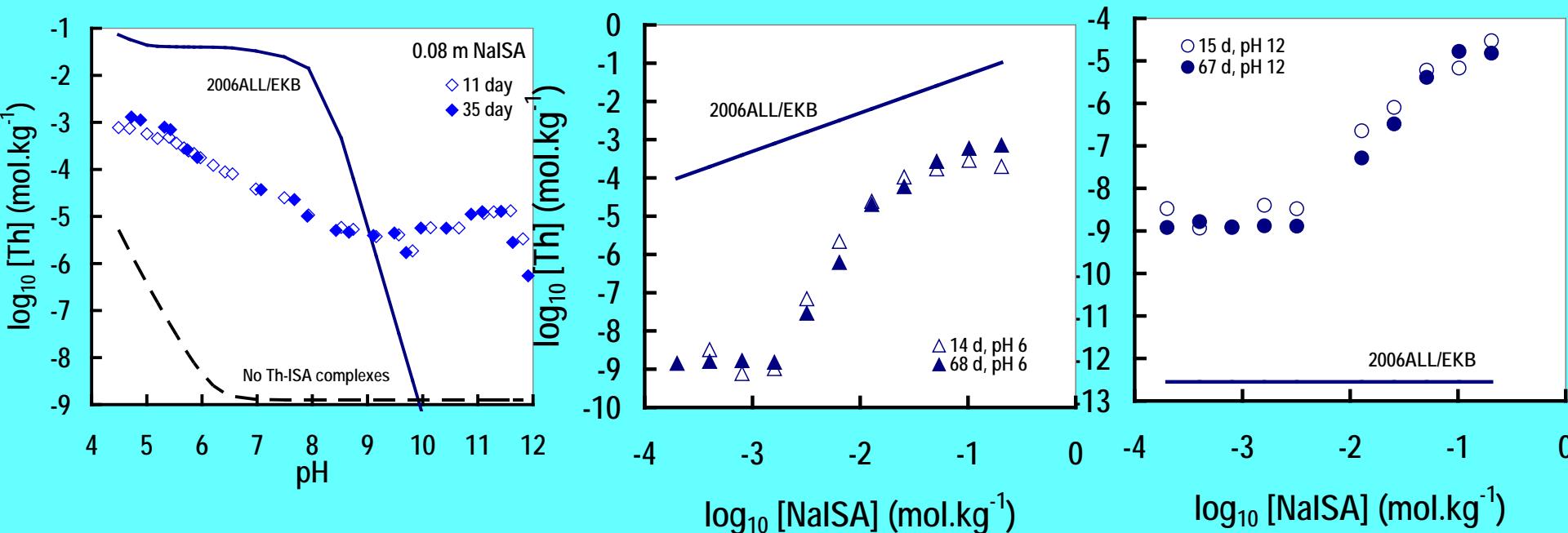
- $\text{ThISA}^{3+}$
- $\text{Th(ISA)}_2^{2+}$
- $\text{Th (ISA)}_3^+$

# Limitations of the 2006 ALL/EKB study

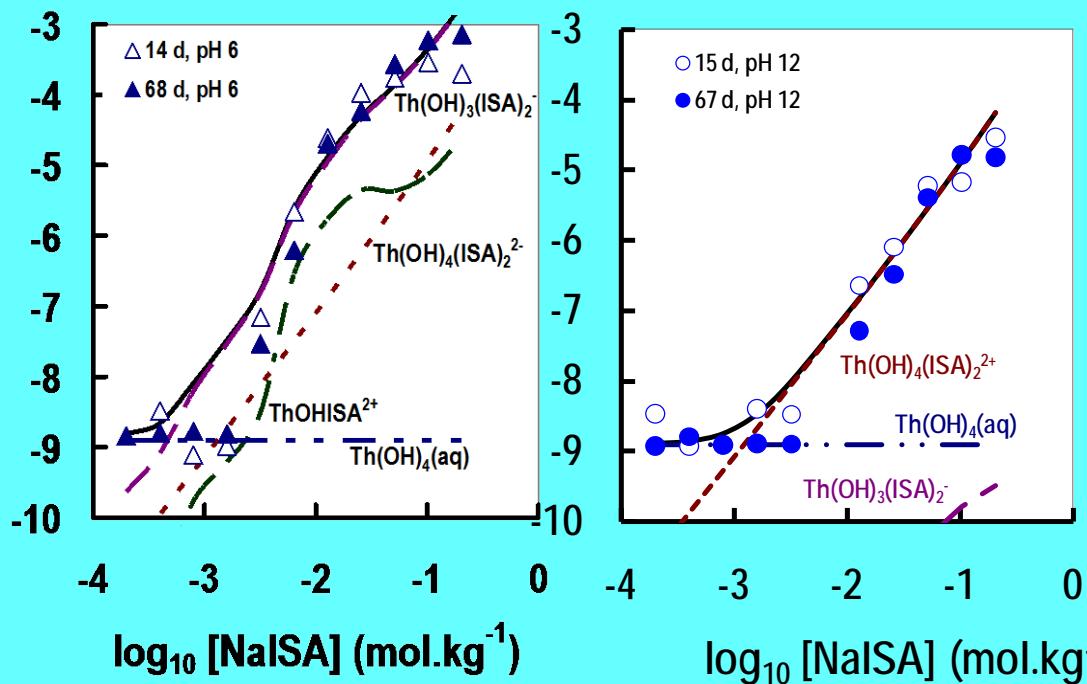
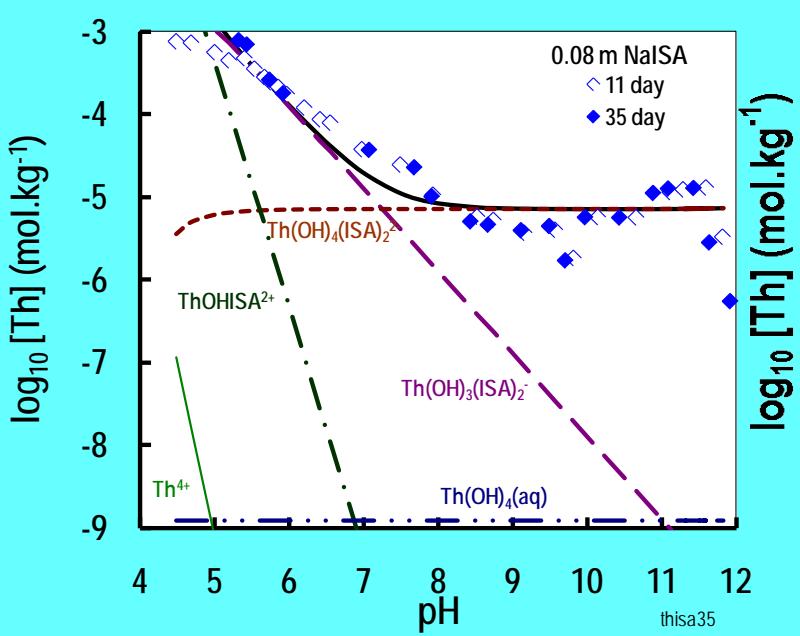
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- Conducted at only one ionic strength (1.0 M)
  - SIT ion-interaction parameters cannot be determined to convert equilibrium constants to zero ionic strength
- Conducted at only one pH (8.3)
  - Structure and type of species may be different at pH values other than 8.3
  - Impossible to differentiate between species they report that have the same ISA dependence but differ in H or OH (e.g., between  $\text{Th}(\text{ISA})_2^{2+}$ , and  $\text{Th}(\text{OH})_3(\text{ISA})_2^-$  or  $\text{Th}(\text{OH})_4(\text{ISA})_2^{2-}$ )
- Extremely unreliable value ( $\log \beta_1 = 12.56 \pm 5.01$ ) for the formation of  $\text{Th}(\text{ISA})^{3+}$

# $\text{ThO}_2(\text{am})$ solubility in 0.08 m NaISA [2009RAI/YUI]: Predictions using 2006ALL/EKB model



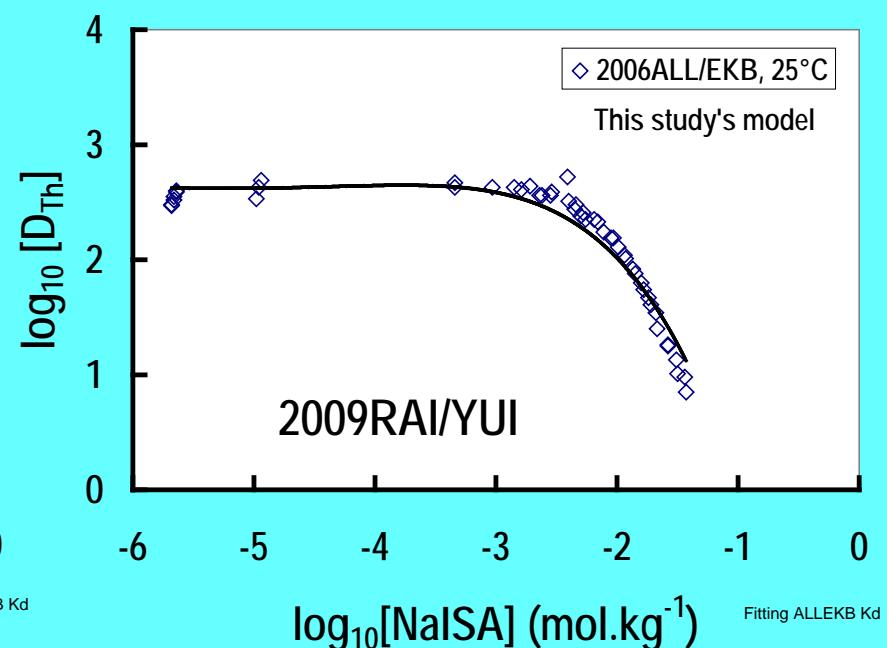
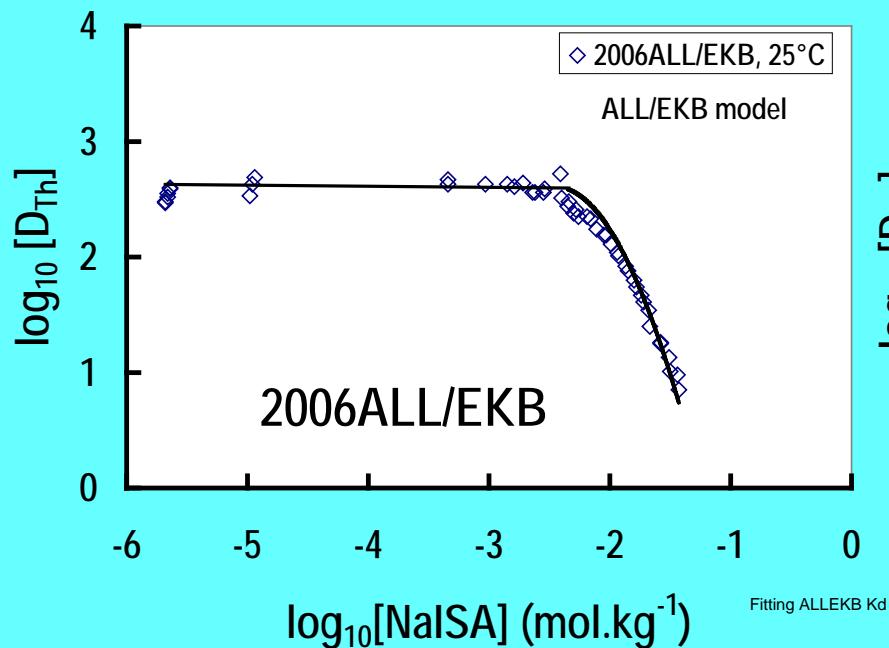
# ThO<sub>2</sub>(am) solubility [2009RAI/YUI]



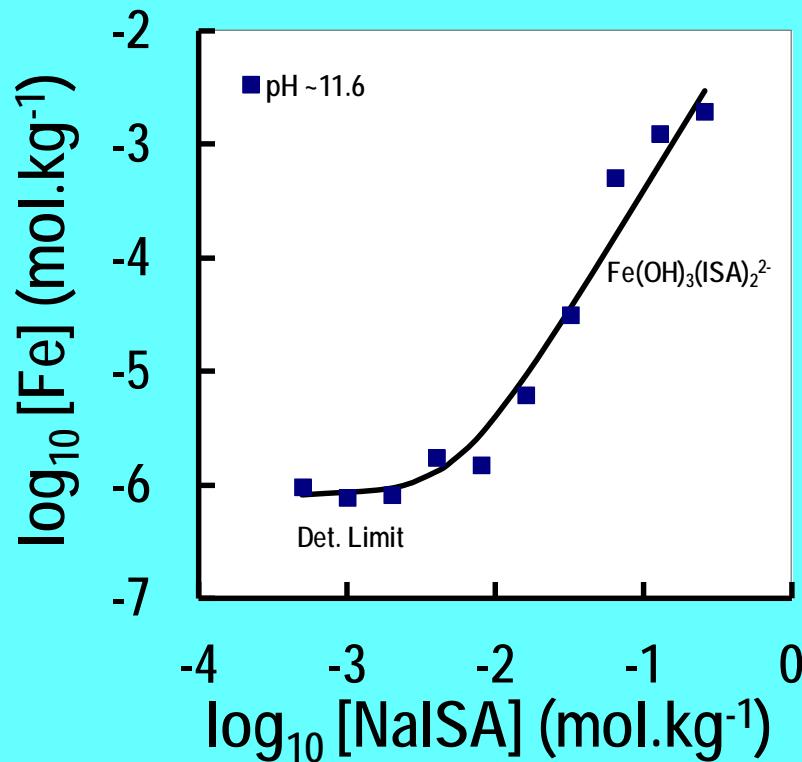
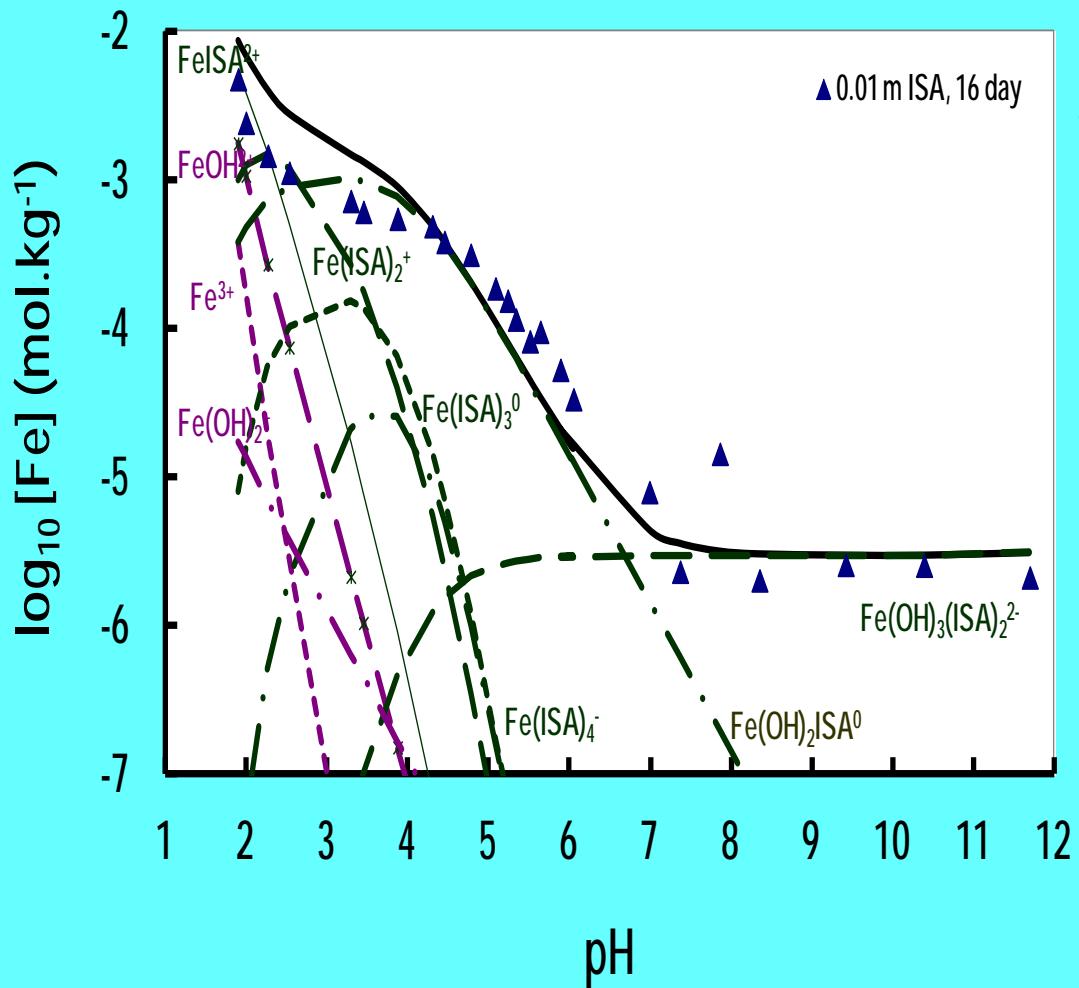
# Important Th-ISA species

2006ALL/EKB	2009RAI/YUI
ThISA <sup>3+</sup>	NR
Th(ISA) <sub>2</sub> <sup>2+</sup>	NR
Th(ISA) <sub>3</sub> <sup>+</sup>	NR
	Th(OH)ISA <sup>2+</sup>
	Th(OH) <sub>3</sub> (ISA) <sub>2</sub> <sup>-</sup>
	Th(OH) <sub>4</sub> (ISA) <sub>2</sub> <sup>2-</sup>
NR = Not required	

# Observed and predicted Th distribution coefficients: 1.05 m NaClO<sub>4</sub>, pH 8.3, 25°C



# $\text{Fe(OH)}_3(\text{s})$ solubility in NaISA [2012RAI/YUI]



# Fe(III)-ISA species based on our studies [2004RAO/GAR and 2012RAI/YUI]

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Important in wide range of pH values

- $\text{Fe(OH)}_2\text{ISA(aq)}$
- $\text{Fe(OH)}_3(\text{ISA})_2^{2-}$

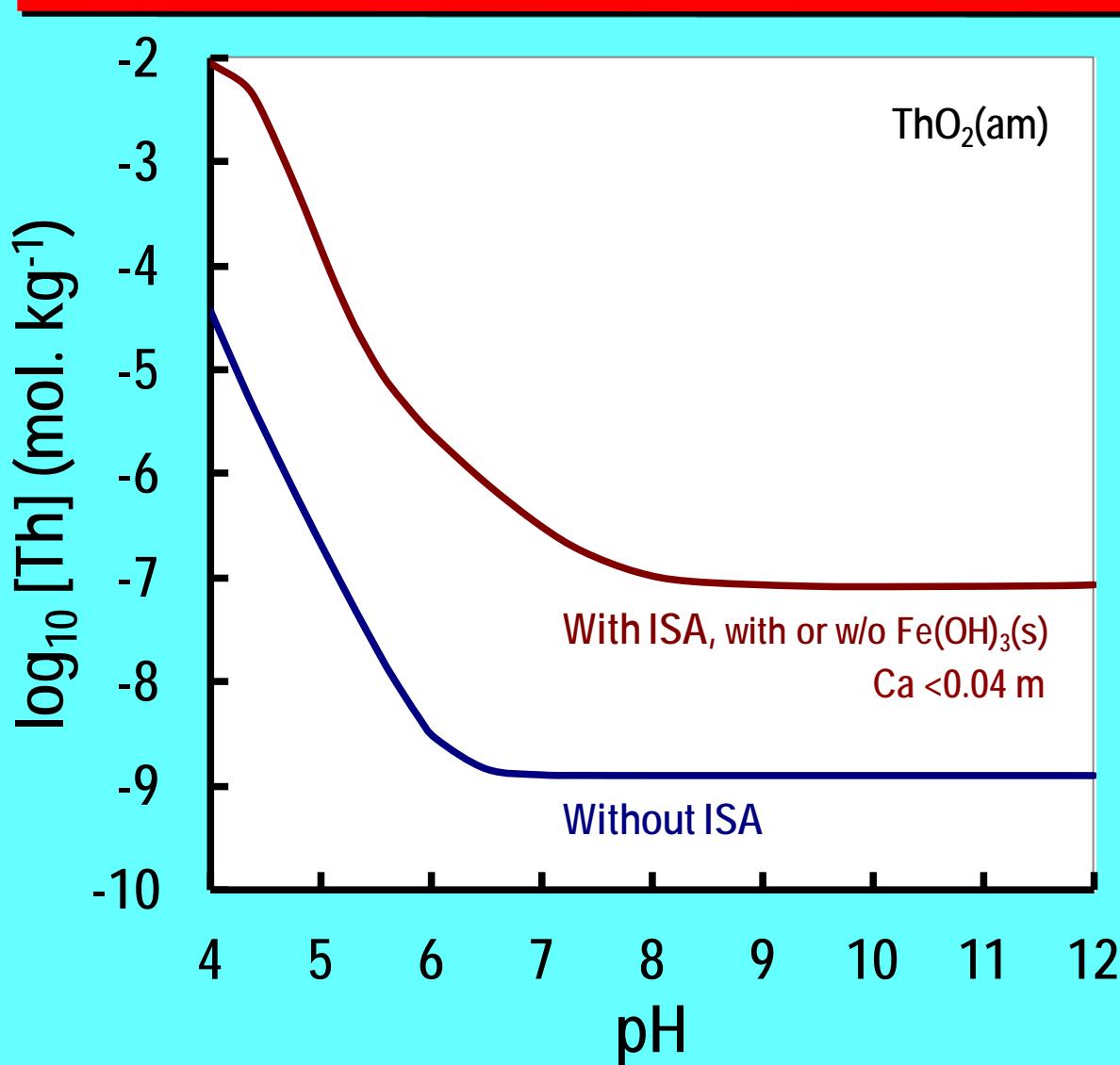
Important only in acidic conditions

- $\text{FeISA}^{2+}$
- $\text{Fe}(\text{ISA})_2^+$
- $\text{Fe}(\text{ISA})_3^0$
- $\text{Fe}(\text{ISA})_4^-$

# Thermodynamic data for the Th-Fe-OH-ISA system

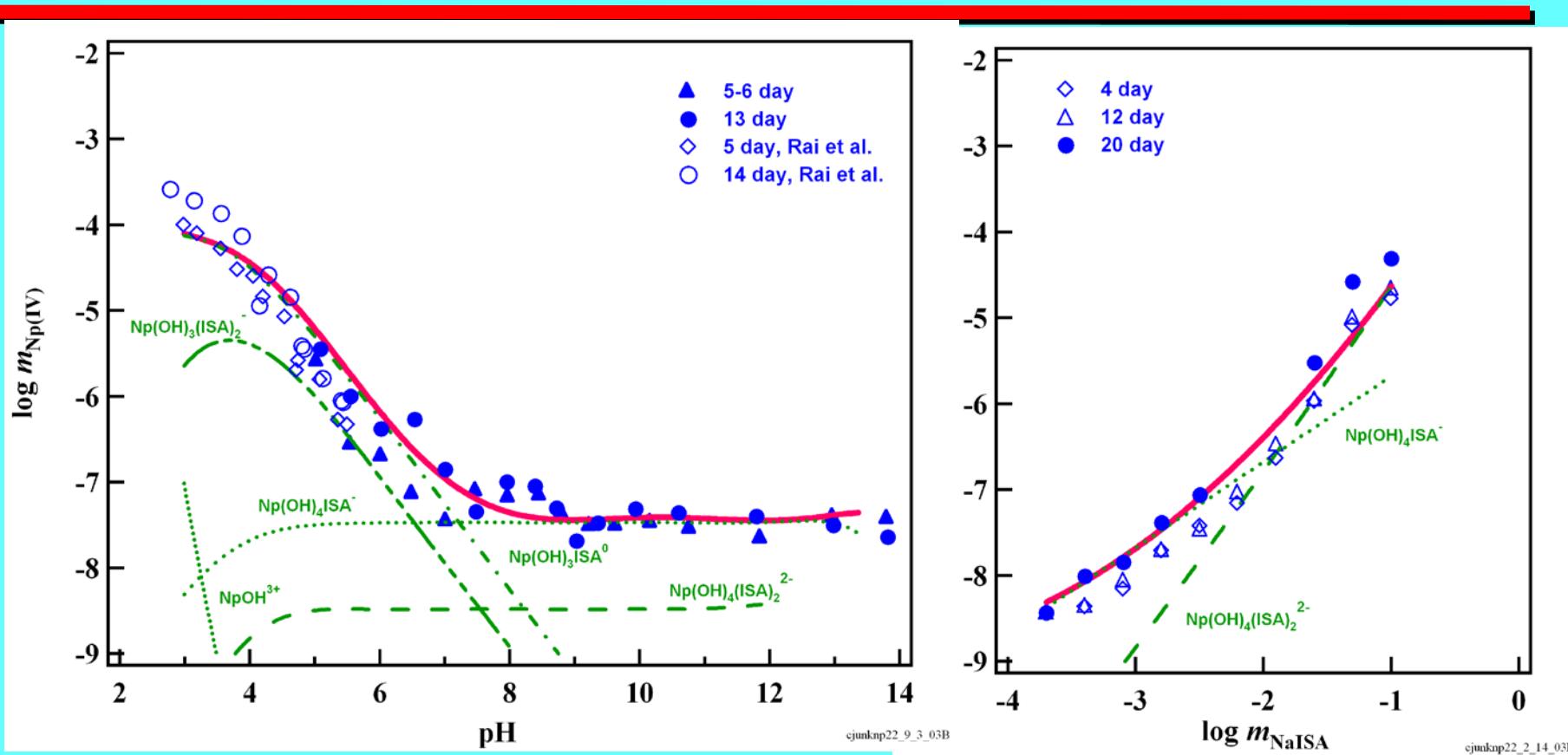
Reaction	$\log_{10} K^0$	Reference
$\text{Fe(OH)}_3(\text{s}) \leftrightarrow \text{Fe}^{3+} + 3\text{OH}^-$	-40.35 ± 0.5	2008RAI/MOO
$\text{Fe}^{3+} + \cdot \leftrightarrow \text{FeOH}^{2+}$	11.81 ± 0.5	2008RAI/MOO
$\text{Fe}^{3+} + 2\text{OH}^- \leftrightarrow \text{Fe(OH)}_2^+$	23.4 ± 1.0	2001SMI/MAR
$\text{ISA}^- + \text{H}^+ \leftrightarrow \text{HISA(aq)}$	4.0 ± 0.5	2005HUM/AND
$\text{Fe}^{3+} + \text{ISA}^- + 2\text{H}_2\text{O} \leftrightarrow \text{Fe(OH)}_2\text{ISA(aq)} + 2\text{H}^+$	1.55 ± 0.38	2012RAI/YUI
$\text{Fe}^{3+} + 2\text{ISA}^- + 3\text{H}_2\text{O} \leftrightarrow \text{Fe(OH)}_3(\text{ISA})_2^{2-} + 3\text{H}^+$	-3.27 ± 0.32	2012RAI/YUI
$\text{Fe}^{3+} + \text{ISA}^- = \text{FeISA}^{2+}$	6.20	2004RAO/GAR
$\text{Fe}^{3+} + 2\text{ISA}^- = \text{Fe}(\text{ISA})_2^+$	10.41	2004RAO/GAR
$\text{Fe}^{3+} + 3\text{ISA}^- = \text{Fe}(\text{ISA})_3^0$	13.10	2004RAO/GAR
$\text{Fe}^{3+} + 4\text{ISA}^- = \text{Fe}(\text{ISA})_4^-$	15.09	2004RAO/GAR
$\text{ThO}_2(\text{am}) + 3\text{H}^+ + \text{ISA}^- = \text{ThOH}(\text{ISA})^- + \text{H}_2\text{O}$	12.5 ± 0.47	2009RAI/YUI
$\text{ThO}_2(\text{am}) + \text{H}^+ + 2\text{ISA}^- + \text{H}_2\text{O} = \text{Th(OH)}_3(\text{ISA})_2^-$	4.41 ± 0.47	2009RAI/YUI

# $\text{ThO}_2(\text{am})$ solubility in 0.01 m NaCl and the presence and the absence of 0.01 m ISA [2009RAI/YUI]



Because of relatively stronger  
Th complexes, Fe(III) and Ca  
have no impact

# NpO<sub>2</sub> solubility in 0.0016 M ISA as a function of pH and at pH 12 and function of ISA [2003RAI/HES]



No changes in Np(IV) concentrations in the presence of Fe(OH)<sub>3</sub>(s) and normal Ca levels

# Summary

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- Outlined general methodology for evaluating complexants for their effect on solubility or use in decontamination
- Using EDTA and ISA as examples I showed:
  - The need for development of reliable data consistent with all of the available data in simple and complex systems
  - The role of both the complexation constants and bare ion activities in PA calculations and selecting decontaminating agents
- The effect of competing metal ions must be considered, which is generally ignored in these kinds of evaluations

# Major references used in presentation

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- Rai, Dhanpat, M. Yui, D. A. Moore. 2012. Isosaccharinate Complexes of Fe(III). *Journal of Solution Chemistry* 41: 1906-1921
- Rai, Dhanpat, Mikazu Yui, D. A. Moore, L. Rao 2009. Thermodynamic Model for  $\text{ThO}_2(\text{am})$  Solubility in Isosaccharinate Solutions. *Journal of Solution Chemistry* 38: 1573 - 1587
- Rai, Dhanpat, D. A. Moore, K. M. Rosso, A. R. Felmy, H. Bolton, Jr.. 2008. Environmental Mobility of Pu(IV) in the Presence of Ethylenediaminetetraacetic acid: Myth or Reality. *Journal of Solution Chemistry* 37: 957 – 986.
- Rao, L., A. Yu. Garnov, Dhanpat Rai, Y. Xia, R. C. Moore. 2004. Protonation and Complexation of Isosaccharinic Acid With U(VI) and Fe(III) in Acidic Solution: Potentiometric and Calorimetric Studies. *Radiochimica Acta* 92: 575-581
- Rai, Dhanpat, N. J. Hess, Y. Xia, L. Rao, H. M. Cho, R. C. Moore, Luc R. Van Loon 2003. Comprehensive Thermodynamic Model Applicable to Highly Acidic to Basic Conditions for Isosaccharinate Reactions with Ca(II) and Np(IV). *Journal of Solution Chemistry* 32: 665-689.
- Cho, H. M., Dhanpat Rai, N. J. Hess, Y. Xia, and L. Rao. 2003. Acidity and Structure of Isosaccharinate in Aqueous Solution: A Nuclear Magnetic Resonance Study. *Journal of Solution Chemistry* 32: 691-702.
- Rai, Dhanpat, H. Bolton, D. A. Moore, N. J. Hess, G. R. Choppin. 2001. Thermodynamic Model for the Solubility of  $\text{PuO}_2(\text{am})$  in the Aqueous  $\text{Na}^+ \text{-} \text{H}^+ \text{-} \text{OH}^- \text{-} \text{Cl}^- \text{-} \text{H}_2\text{O}$ -Ethylenediaminetetraacetate System *Radiochimica Acta* 89: 67-74

# Pitzer ion-interaction parameters (Rai et al. 2008)

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Species	$\beta^{(0)}$	$\beta^{(1)}$	$C^\phi$
$\text{Na}^+ - \text{Pu(OH)EDTA}^-$	-0.2345	0.29	0.059
$\text{Na}^+ - \text{Pu(OH)}_2\text{EDTA}^{2-}$	-0.1262	1.74	0.054
$\text{Na}^+ - \text{Pu(OH)}_3\text{EDTA}^{3-}$	0.59	5.39	0.00
$\text{Na}^+ - \text{FeEDTA}^-$	-0.2345	0.29	0.059
$\text{Na}^+ - \text{Fe(OH)EDTA}^{2-}$	-0.1262	1.74	0.054

# SIT Ion-interaction parameters determined by [2012RAI/YUI]

Species	$\epsilon(\text{kg}\cdot\text{mol}^{-1})$
$\text{Na}^+, \text{Fe(OH)}_3(\text{ISA})_2^{2-}$	-0.125
$\text{Na}^+, \text{Th(OH)}_3(\text{ISA})_2^-$	-0.07
$\text{Na}^+, \text{Th(OH)}_4(\text{ISA})_2^{2-}$	-0.125
$\text{FeISA}^{2+}, \text{ClO}_4^-$	0.4
$\text{Fe}(\text{ISA})_2^+, \text{ClO}_4^-$	0.27
$\text{Fe}(\text{ISA})_3^0, \text{ClO}_4^-$	0.00
$\text{Fe}(\text{ISA})_4^-, \text{ClO}_4^-$	-0.07

# Thermodynamic interpretations of $\text{PuO}_2(\text{am})$ solubility data (Rai et al. 2008)

